Region

Oil is cracked in Reactor and does not travel to Hx or Gx

- 600 ton fluidized bed of 50 300 micron coke particles at 510 530°C
 - 7 meters diameter, 70 meters high
 - fluidization by steam and product vapors
- Reactor is fed at 6 elevations; several feed nozzles per ring
- Product yields

-														

Naphtha and gasoils 55 - 65 %

- Coke 25 - 30 %



R62.00

- Heat input via coke transport from heater, 2000 ton/hr, dT= 100 °C
- Tight temperature control
 - reactor too hot: liquid yield loss due to over cracking
 - reactor too cold : more wall coke or even bogging
- Reactor products leave reactor via cyclones to scrubber
 - entrained coke particles are scrubbed with liquid feed in scrubber
 - preheat feed and control FBP heavy gasoil product / recycle



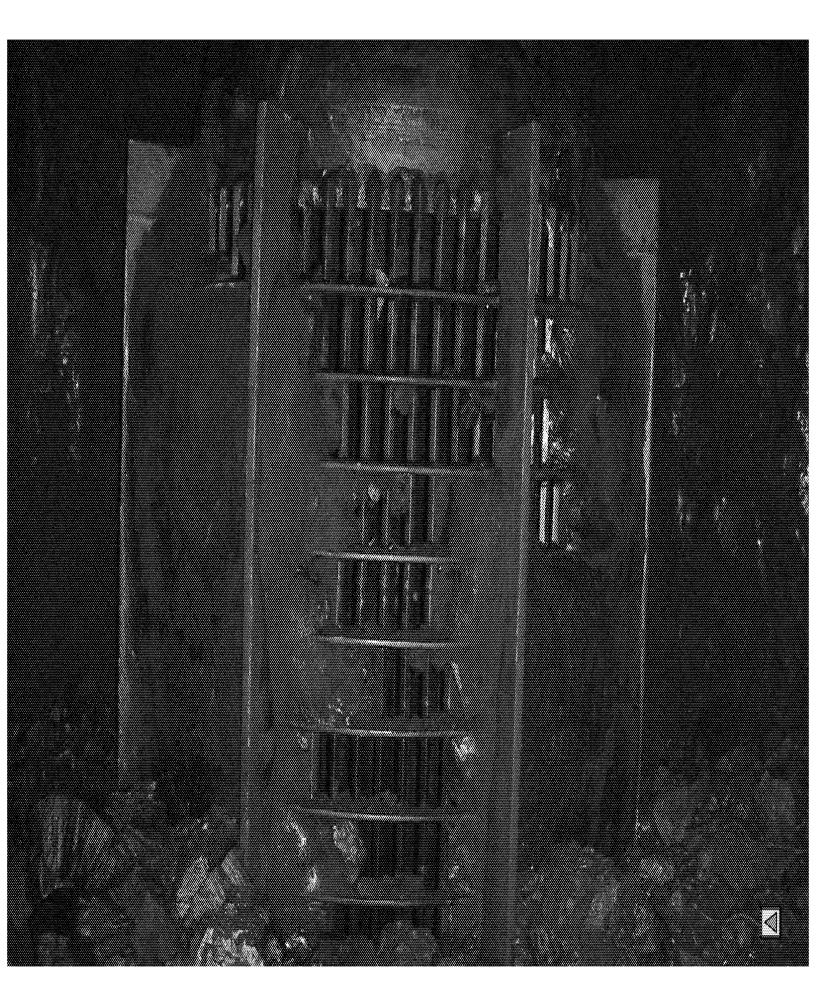
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What to watch for during operation?

- Bogging (too low Reactor temperature)
- Blockage of coke transport to/from heater
- Coke entrainment / sticky coke
- High vessel wall temperature
- Hydrocarbon carry under



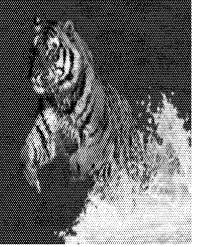






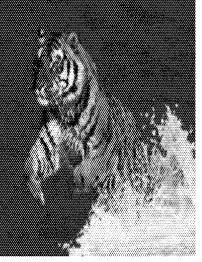
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- 600 630°C bed, fluidized by LJG from Gasifier
- Cools LJG and transfers heat to cold reactor coke
- Temperature fine tuning with a little bit of air
- Mechanically complicated vessel
 - many transfer lines and 14 two stage cyclones
 - internal gas distribution/bed support grid exposed to high temperatures
 - "quench tee" and "sugar scoop"



Heater Maintenance Challenges Grid Can Orifice Erosion

- Orifices center caps plug with coke lumps
- Orifices of outer caps erode in 1 run
- Replace entire can is quickest repair option
- Repairs on critical path of site turnaround
- Splash plates and birdcages
- Grid redesign idea

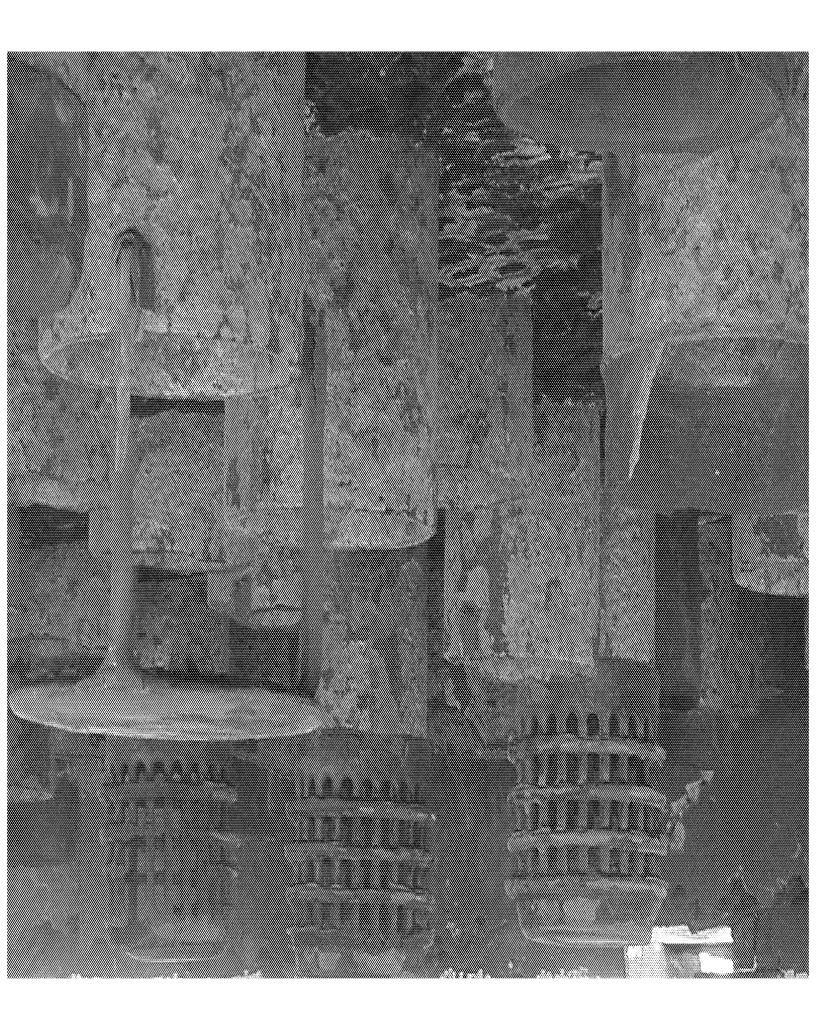












Heater Maintenance Challenges Carburization of Stainless Steel

- All internals stainless steel: 18% Cr/8% Ni
- Temperature range 590 635°C
- Gas contains H₂, CO and H₂S
- CO reacts with Cr to chromium carbides
- H₂S corrosion of steel due to reduced Cr content
- Cyclones replaced in last turnaround



